

# A high-resolution large-eddy simulation framework for wildland fire predictions using TensorFlow

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## ABSTRACT

**Background.** Wildfires are becoming more severe, so we need improved tools to predict them over a wide range of conditions and scales. One approach towards this goal entails the use of coupled fire/atmosphere modelling tools. Although significant progress has been made in advancing their physical fidelity, existing tools have not taken full advantage of emerging programming paradigms and computing architectures to enable high-resolution wildfire simulations. **Aims.** The aim of this study was to present a new framework that enables landscape-scale wildfire simulations with physical representation of combustion at an affordable cost. **Methods.** We developed a coupled fire/atmosphere simulation framework using TensorFlow, which enables efficient and scalable computations on Tensor Processing Units. **Key results.** Simulation results for a prescribed fire were compared with experimental data. Predicted fire behavior and statistical analysis for fire spread rate, scar area, and intermittency showed overall reasonable agreement. Scalability analysis was performed, showing close to linear scaling. **Conclusions.** While mesh refinement was shown to have less impact on global quantities, such as fire scar area and spread rate, it benefits predictions of intermittent fire behavior, buoyancy-driven dynamics, and small-scale turbulent motion. **Implications.** This new simulation framework is efficient in capturing both global quantities and unsteady dynamics of wildfires at high spatial resolutions.

**Keywords:** fire/atmospheric coupling, fire management, fire propagation, large-eddy simulation, tensor processing units, TensorFlow, wildfire modelling, wildland fire prediction.

## Introduction

The frequency and severity of wildfires has increased profoundly over the past decades (Westerling *et al.* 2006; Jolly *et al.* 2015; Abatzoglou and Williams 2016) because of several confounding factors, including changes in fire suppression and fire management, extent of the wildland–urban interface, and climate. Many regions are experiencing extended fire seasons and increased annual burn area (Westerling 2016; Parks and Abatzoglou 2020). The increased fire severity causes significant ecological and economical losses (Thomas *et al.* 2017) and health burdens (Burke *et al.* 2021), which create challenges for environmental planning and fire management (Hessburg *et al.* 2021).

To address the need for predictive methods that can guide fire management, enable landscape management, inform policy decisions, and support scientific inquiry, simulation techniques of varying physical fidelity, computational complexity, and accuracy have been developed (Sullivan 2009a, 2009b, 2009c). Accurately predicting wildfire dynamics across a wide range of wildland fire conditions requires the consideration of complex fire–atmosphere interactions, including the coupling between meteorology, heat transfer, turbulence, and combustion (Liu *et al.* 2019). To capture these coupling effects, physics-based models are needed (Bakhshai and Johnson 2019).

Physics-based simulation tools are divided into two major categories based on scale (Bakhshaii and Johnson 2019). One of the categories focuses on predicting meso-scale wildland fire behaviour. By integrating empirical (Rothermel 1972) or algebraic physics-inspired (Balbi *et al.* 2009) fire-spread models into numerical weather prediction models, these simulation approaches enable the prediction of fire-spread behaviour on scales spanning more than 100 km in real time. Examples of this category of models include WRF-SFIRE (Mandel *et al.* 2011), CAWFE (Coen 2013), WRF-Fire (Coen *et al.* 2013), and MesoNH-ForeFire (Filippi *et al.* 2011). Although these approaches have been shown to capture the global fire behaviour, such as the rate of spread (ROS), their coarse spatial resolution limits the accurate prediction of fire intermittency and turbulent fire dynamics, which is critical for simulating unsteady fire events (Finney *et al.* 2015; Viegas *et al.* 2022).

The second category of physics-based simulation approaches focuses on fires at the micro-scale. In these approaches, the hydrodynamics are represented with large-eddy simulations (LES) or Reynolds-averaged Navier-Stokes (RANS) simulations, and is fully coupled with the fire dynamics through the use of a fire model that represents the chemical reactions. Representative models of this category are the CNRS Fuel Beds Simulator (Porterie *et al.* 2000), FIRETEC (Linn *et al.* 2002), WFDS (McGrattan *et al.* 2006), FireFOAM (Wang *et al.* 2011), and FireStar3D (Morvan *et al.* 2018). Although these models capture the unsteady fire-atmosphere interactions, their high computational cost has constrained the spatial extent and duration of fire predictions (Sullivan 2009a; Coen *et al.* 2020). As such, the use of these models in predicting the behaviour of large wildfires remains challenging.

With the recent advancements in computer technologies, including hardware architectures and software stacks, opportunities arise to significantly improve the efficiency of physics-based wildfire simulations. Therefore, the objective of this work is to develop and validate a physics-based coupled fire/atmosphere solver, named SWIRL-FIRE, for large-scale high-fidelity wildland fire simulations. This solver is based on the open-source low-Mach hydrodynamic simulation framework SWIRL-LM (Wang *et al.* 2022a), and integrates sub-models of FIRETEC (Linn and Cunningham 2005) to represent the combustion and multi-phase interaction with vegetation, thereby accounting for the coupling between the fire and the atmosphere. This simulation framework leverages the TensorFlow programming paradigm (Abadi *et al.* 2015) and tensor processing units (TPUs), which were developed for machine learning (ML) and scientific computing (Jouppi *et al.* 2021). TensorFlow enables ML capabilities, but the focus of the present study is on evaluating the physical model implementation and spatial resolutions; the utilisation of ML will be addressed in future work. Access to this TPU computing hardware is available through the Google Cloud Platform, and the code is publicly

available through GitHub (Wang *et al.* 2022a). The accelerated numerical computations by the new hardware allow us to simulate meso-scale wildfires at homogeneous spatial resolution of  $O(10^{-1})$  m, with  $O(10^9)$  m grid points at an affordable operation cost. We evaluate this modelling tool in application to a prescribed fire experiment, FireFlux II (Clements *et al.* 2019), with specific attention paid to the effect of spatial resolution on representing the fire dynamics. The importance of mesh resolution and domain size has been discussed in previous studies (Moinuddin *et al.* 2018), showing that local refinement of the burnable fire region is necessary to obtain converged fire-spread predictions.

The remainder of this manuscript has the following structure. The next section presents methods that are used to construct the simulation framework, including the mathematical model, solution algorithm, and implementation. The experiment and computational setup section introduces the simulation setup based on the FireFlux II experiment. Results are presented in the subsequent section, discussing comparisons with experimental data and sensitivity analysis with respect to the mesh resolution. Concluding remarks are provided in the last section.

## Methods

### Mathematical model and solution algorithm

In this work, we model the spatio-temporal dynamics of wildland fires using an LES approach, in which the governing equations for the gas-phase are described by the solution of the Favre-filtered conservation equations for mass, momentum, oxygen mass fraction, and potential temperature. To account for subgrid-scale effects, arising from the turbulent stresses and turbulent scalar transport, we employ the Smagorinsky-Lilly model (Lilly 1962). The combustion of the solid fuel is modelled by a one-step mixing-limited oxidation reaction, and energetic impacts of moisture evaporation are accounted for. The implementation of the combustion model follows the work of Linn *et al.* (2002) and is summarised in Appendix 1. Different from FIRETEC, which adopts a fully compressible formulation, the present work solves the governing equations with a low-Mach number approach with prescribed hydrostatic reference state. This enables advancing the solution at larger time-step sizes by removing the dependence on the acoustic wave propagation.

The governing equations are solved on a three-dimensional Cartesian coordinate system using a finite-difference discretisation. All spatial operators are discretised on a collocated mesh, and time-staggering is employed for the temporal discretisation. Along each direction the mesh is equidistant. The coupled system of equations is solved using a predictor-corrector method with a time-explicit iterative scheme. Further details on the numerical discretisation, solution algorithm, and convergence properties can be found in Wang *et al.* (2022a).

## TPU computing architecture and implementation

All simulations presented in this work are performed on the TPUv4 computing architecture. Each chip in this computing architecture has two tensor compute cores that are optimised for dense linear algebra operations, such as matrix–matrix multiplications that are performed by a specially designed processing unit called matrix-multiplication unit (MXU), providing a peak throughput of 275 teraflops per chip. Each chip has 32-GiB high-bandwidth memory for fast memory access. A total of 4096 chips (8192 cores) are connected through a high-speed, three-dimensional toroidal network for low-latency data communication between cores. The TPUv4 architecture supports 8-bit arithmetic natively, and high-precision arithmetic is available through software emulations. Simulations in the present study are performed with single precision for the desired balance between computational efficiency and numerical accuracy. We implemented the simulation framework with TensorFlow, which offers specific advantages by utilising existing libraries and the just-in-time compilation to optimise the performance on TPU architectures (Wang *et al.* 2022a).

## Experiment and computational setup

To evaluate the accuracy and performance of the proposed simulation framework, we consider the FireFlux II experiment as a benchmark configuration. In the following, we summarise the experiment and describe the computational setup that is employed to simulate this experiment.

### Experimental setup

The FireFlux II experiment (Clements *et al.* 2019) is a prescribed grassland fire on a flat-field prairie site. This experiment included both ambient fuel and wind observations as well as fire-spread. Based on atmospheric measurements prior to ignition, a west–northwest wind with an average 10-m wind speed of 8.5 m/s was reported. The mean temperature was 16°C. The unit-average fuel loading was reported as 0.64 kg/m<sup>2</sup>, with a variation between 0.41 and 0.81 kg/m<sup>2</sup> due to fine-particle heterogeneities from the upper- and lower-layer grasses, forbs, and shrubs.

The field was instrumented to simultaneously measure the development of the head fire and atmospheric conditions. This instrumentation included meteorological towers for locally measuring near-surface momentum, heat transport, wind velocity, and sonic temperature. Discrete measurements were performed at the main tower at measurement heights of 5.8, 10, 20, and 43 m above the ground level (AGL). The fire spread was measured using a total of 20 thermocouple-based HOBO temperature data loggers placed at the soil surface and arranged on a grid

to record the fire-spread rate. Further details on the measurements, instrumentations, and data acquisition can be found in Clements *et al.* (2019). Available measurements are used to compare our simulation results.

### Computational setup

In the present work, we consider experimentally reported conditions of the FireFlux II experiment, and no attempts were made to tune model parameters or operating conditions to match experimental results. The conditions and properties used in our simulations are summarised in Table 1.

To represent the fire spread over the course of the experiment, we adopted a prismatic domain with size 1000 × 500 × 1200 m<sup>3</sup> in streamwise (x), spanwise (y), and vertical (z) directions, respectively. The streamwise direction is aligned with the mean wind from west–northwest direction. The height of the domain is selected to capture the atmospheric boundary layer. A parametric study was performed by increasing the lateral extent of the domain to 1000 m, showing no appreciable changes in the fire behaviour.

To represent the shear stress and heat flux of the atmospheric boundary layer, the bottom-surface boundary is modelled with the Monin–Obukhov similarity theory (Stoll and Porté-Agel 2006). A Rayleigh damping layer (Klemp and Lilly 1978) is used within the top 10% of the computational domain. For a generic variable  $\phi$  with a background value  $\phi_0$ , the Rayleigh damping term is computed as  $f_{\phi, RD} = -\beta_{RD}(\phi - \phi_0)$ , where  $\beta_{RD}$  is a relaxation coefficient, which is a function of the depth ( $\zeta$ ) into the total thickness of the Rayleigh damping layer ( $\zeta_0$ ). In our simulations,  $\beta_{RD}(\zeta) = (20\Delta t)^{-1} \sin^2\left(\frac{\pi \zeta}{2 \zeta_0}\right)$  (Klemp and Lilly 1978), with  $\zeta_0 = 0.1l_z$  and  $\zeta \in [0, \zeta_0]$ , and  $\Delta t$  is the step size in the simulation. This model is employed to prevent entrainment into the flow domain or the generation of unphysical flow structures at the top of the computational domain. Along the lateral sides of the computational domain, adiabatic and free slip boundary conditions are enforced.

Boundary conditions at the inflow are prescribed by a time-dependent turbulent inflow profile. These inflow conditions were obtained by performing an auxiliary flow

**Table 1.** Physical parameters in the simulations.

Operating condition (unit)	Value
10-m wind speed (free stream) (m/s)	8.5
Wind direction (with respect to y-direction) (°)	−10.0
Fuel type	Tall grass
Unit fuel load (kg/m <sup>2</sup> )	0.6
Fuel distribution	Homogeneous
Fuel height (m)	1.5
Moisture content (%)	14.2

simulation in the computational domain without igniting the fire (Appendix 2), assuming that the atmospheric boundary layer is neutrally stratified. To obtain a fully developed turbulent boundary layer, we simulate a temporally evolving boundary layer by employing periodic boundary conditions in streamwise direction (Linn et al. 2013). To match the experimental condition, the free-stream wind speed is set to the experimentally reported 10-m wind of 8.5 m/s. After advancing this simulation over 100 flow-through times (FTTs), defined as  $t_{\text{FTT}} = l_x/U_\infty$  (with  $l_x$  being the length of the domain and  $U_\infty$  the free-stream wind speed), to establish a statistically stationary turbulent boundary-layer profile, we extract the three-dimensional velocity field at the  $y$ - $z$  cross-section 500 m from the inlet of the domain for 500 s, corresponding to 4.25 FTTs. An analysis of the atmospheric boundary layer is presented in Fig. A1.

To perform the fire simulations, we initialised the flow field with the last snapshot from the auxiliary turbulent inflow simulation. The potential temperature profile that is used to initialise the flow field was obtained by interpolating the sounding data collected in the morning of the day of the experiment (Clements et al. 2019).

To examine effects of the horizontal mesh resolution on the fire-spread behaviour, we consider four different meshes in which the vertical resolution is kept constant at  $\Delta_z = 0.5$  m, and the resolution in the horizontal direction is successively refined from  $\Delta = 4$  m (Case A), to  $\Delta = 2$  m (Case B), to  $\Delta = 1$  m (Case C), and to  $\Delta = 0.5$  m (Case D). With this, our finest mesh (case D) has a total of  $4.295 \times 10^9$  grid points. In addition, to examine effects of the vertical resolution, we performed two additional mesh refinement studies in which the vertical mesh resolution for Case C was refined to  $\Delta_z = 0.25$  and  $\Delta_z = 0.125$  m. These two cases are denoted as Case C.1 and Case C.2, respectively. The resulting mesh configurations for all cases are summarised in Table 2.

In this study, each fire simulation was advanced over 200 s (1.7 FTT) before ignition to establish a statistically stationary flow field. To replicate the experimental ignition procedure, fire ignition was then initiated by tracing two

high-temperature ignition kernels along the lateral direction at a tilting angle of  $10^\circ$  (and a speed of 0.8 m/s for 110 s). The simulations ran for another 200 s to cover the full duration of the experimental observations.

## Results

In this section, we discuss the simulation results. Starting with a qualitative description of the fire behaviour to generate intuition, we continue with quantitative comparisons against available measurements from the FireFlux II experiment. This is followed by statistical analysis, the examination of the dynamic behaviour, and a discussion about the computational efficiency of this simulation framework.

### Instantaneous fire-spread behaviour

Fig. 1 shows instantaneous snapshots for temperature (left column) and  $Q$ -criterion (right column) of the fire spread between 120 and 200 s after ignition. Provided by the ambient wind, a head fire dominates the fire propagation, with narrow fire flanks due to misalignment of the fire-spread rate with the ambient wind direction. In addition, the formation of a plume with counter-rotating vortex pairs is visible as indicated by the isosurface of the oxygen mass fraction of 0.1. This is a result of the large ambient wind speed, which suggests a fast dispersion of the combustion products in the downstream direction relative to the spreading of the ground fire. To illustrate the interaction between the turbulence from the atmospheric boundary layer and the fire front, we evaluate the  $Q$ -criterion. This criterion is computed as the second invariant of the velocity gradient tensor and quantifies the balance between strain and vorticity (Chong et al. 1990). The three panels in the right column of Fig. 1 show that large-scale vortical structures are formed at the periphery of the fire front, resulting in the formation of counter-rotating vortices that are advected into the upper atmosphere.

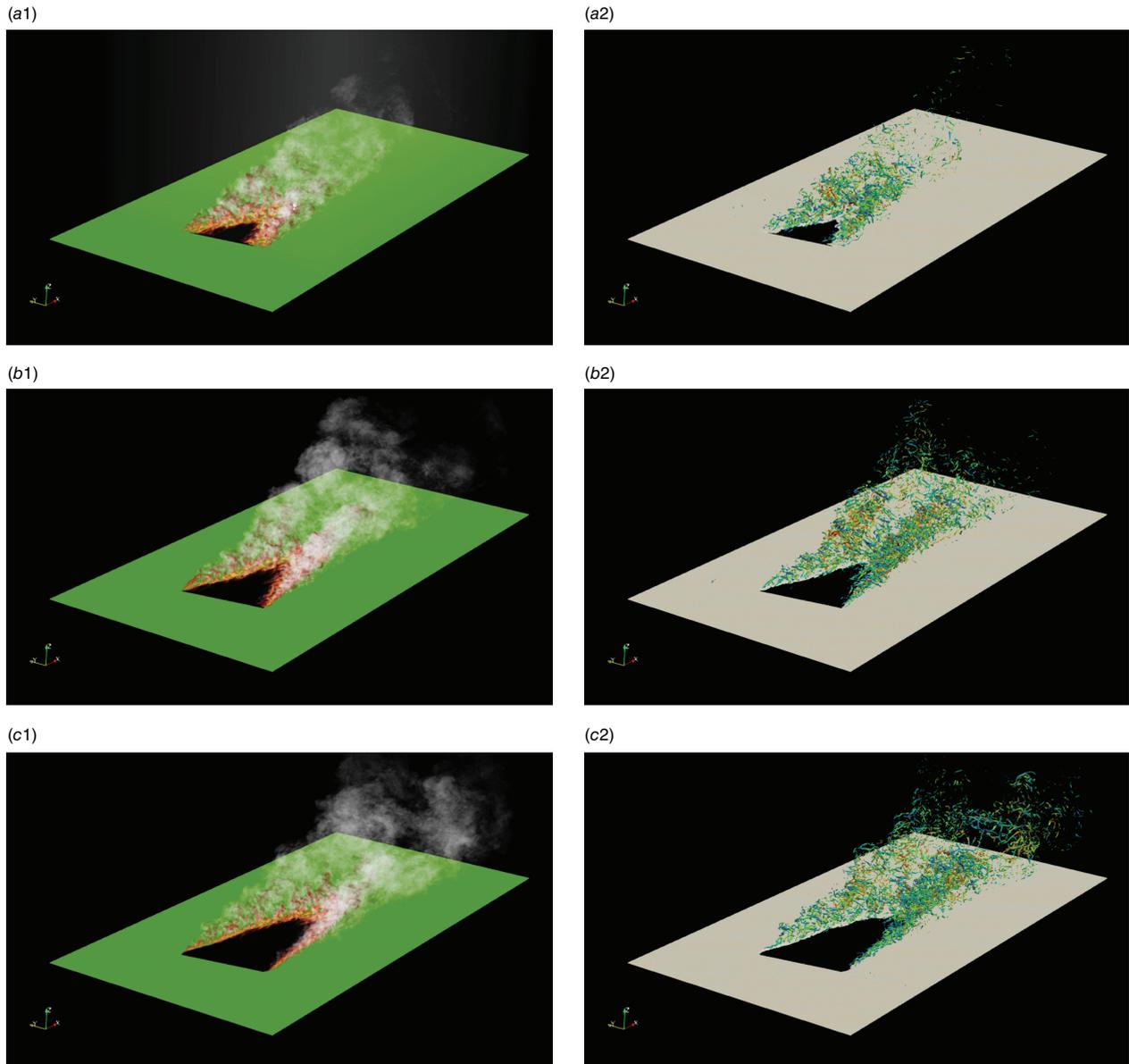
The interaction between the fire and the turbulence is further illustrated in Fig. 2, showing contours of the potential temperature and vorticity in a slice perpendicular to the lateral direction. The height of the fire plume grows linearly in the upwind direction, forming an apparent angle of  $50^\circ$  with respect to the vertical direction. An average fire tilt angle of  $30^\circ$  is observed in the flame zone, and this value will be used to compute the flame length in the subsequent section. We also observe an updraft in the fire plume due to the buoyancy induced by the formation of hot products, as indicated by the velocity streamlines.

### Comparisons with FireFlux II experiment

Comparisons of the fire spread behaviour for the six simulations of increasing spatial resolution are presented in Fig. 3,

**Table 2.** Mesh resolution and mesh size used for the FireFlux II simulations.

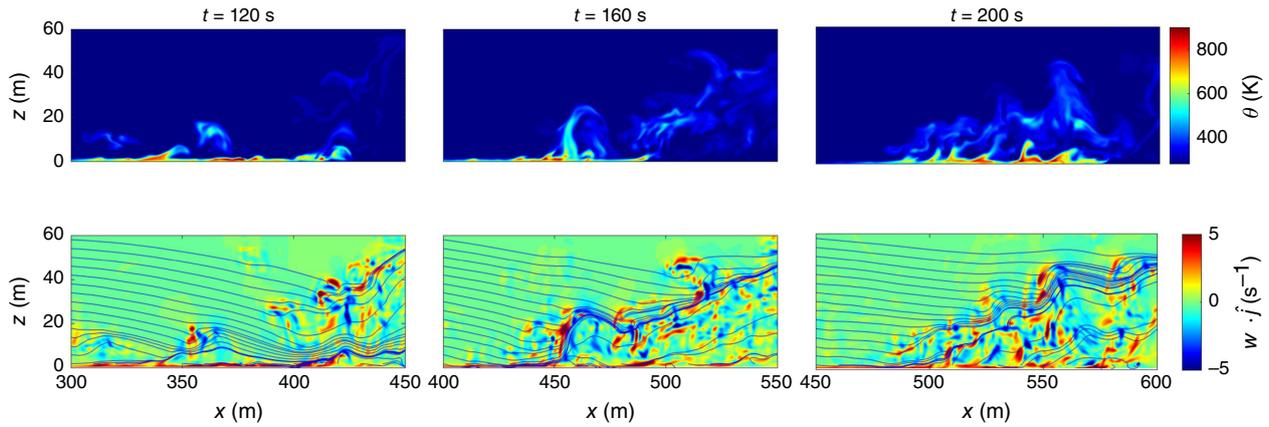
Case	Mesh resolution ( $\Delta \times \Delta \times \Delta_z$ ) (m <sup>3</sup> )	Mesh size ( $N_x \times N_y \times N_z$ )	Total mesh size
A	$4 \times 4 \times 0.5$	$256 \times 128 \times 2048$	$6.711 \times 10^7$
B	$2 \times 2 \times 0.5$	$512 \times 256 \times 2048$	$2.684 \times 10^8$
C	$1 \times 1 \times 0.5$	$1024 \times 512 \times 2048$	$1.074 \times 10^9$
C.1	$1 \times 1 \times 0.25$	$1024 \times 512 \times 4096$	$2.147 \times 10^9$
C.2	$1 \times 1 \times 0.125$	$1025 \times 512 \times 8192$	$4.295 \times 10^9$
D	$0.5 \times 0.5 \times 0.5$	$2018 \times 1024 \times 2048$	$4.295 \times 10^9$



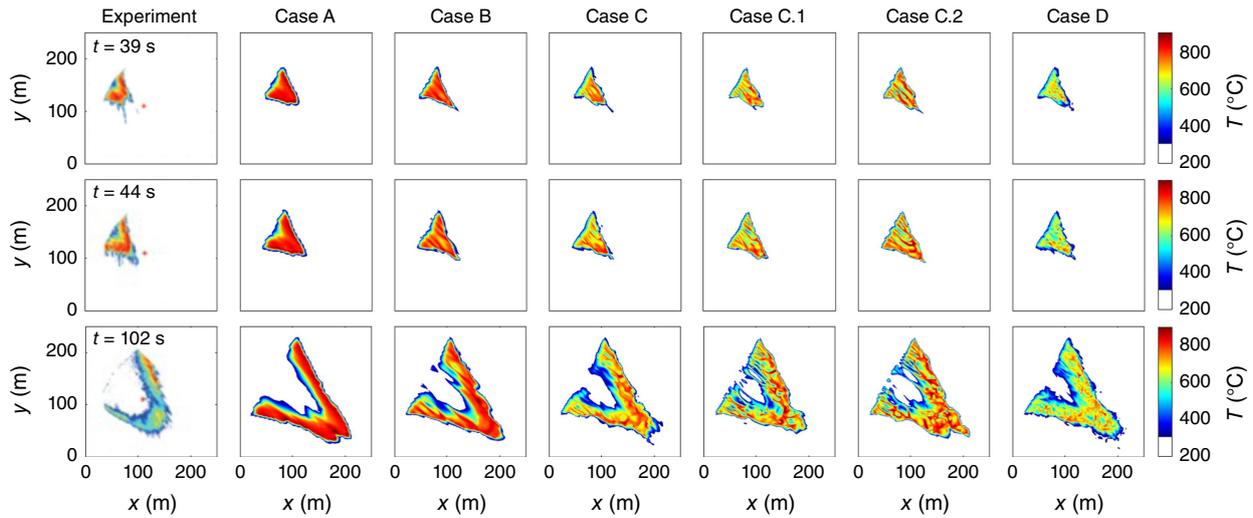
**Fig. 1.** 3D visualisation of the simulated fire at (a)  $t = 120$  s, (b)  $t = 160$  s, and (c)  $t = 200$  s after ignition. Left column: temperature and proxy of emission plume (indicated by the isocontour of the oxygen mass fraction of 0.1); right column: isosurface of the  $Q$ -criterion (for a value of  $1 \text{ s}^{-2}$ ) colour-coded by the streamwise velocity magnitude. Results are shown for case D with 0.5 m horizontal resolution. Entire domain is shown.

showing the gas-phase temperature at 1.5 m AGL for three different time instances, corresponding to 39, 44, and 102 s after ignition. To provide a qualitative comparison with experimental observations, we show geo-rectified infra-red (IR) images in the first column at the same time instances. Overall, the fire topologies predicted with different mesh resolutions show reasonable qualitative agreement with IR measurements, showing similar location and direction of the heading fire as well as the rate of spread. We note that a direct comparison with experiments is not possible due to the lack of information about the IR-image processing.

Therefore, in Fig. 3, we focus on a qualitative comparison with the experiment only. Results from Cases A and B show highly diffusive flame structures with higher gas phase temperatures compared with the other cases. Among Cases C, C.1, and C.2 with a horizontal resolution of 1 m, we see similar fire structures with more corrugations in the fire zone, suggesting that the finer mesh resolution is able to better resolve the fine-scale turbulent structures and its interaction with the fire. Different vertical resolutions among these three cases do not show significant sensitivities in terms of the fire-front location. Case D has a broader



**Fig. 2.** Potential temperature (top) and spanwise vorticity component at  $t = 200$  s after ignition. Contours are plotted at the mid-plane normal to the lateral axis ( $y = 250$  m). Panels show a narrow region of the larger domain around the fire zone.



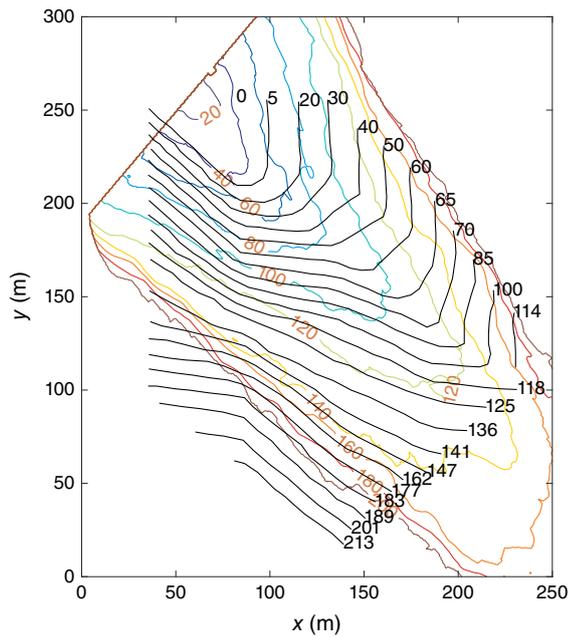
**Fig. 3.** Qualitative comparison of gas-phase temperature field between the experiment and simulations at 1.35 m AGL. The three rows show results for 39 s (top), 44 s (middle), and 102 s (bottom) after ignition, which corresponds to the times of 15:04:47, 15:04:52, and 15:05:50 hours, respectively, in the experiment (Clement et al. 2019). The first column is a reference from the experiment. Columns 2–7 are from simulations of Cases A, B, C, C.1, C.2, and D, respectively.

flame zone than all other cases, with more fine-scale structures that are represented by regions of higher gas phase temperature inside the flame zone.

The prediction of the fire-spread behaviour is further examined by comparing predictions with experimentally measured isochrones for fire-front arrival. Results from this comparison are shown in Fig. 4. The black contours are obtained from the interpolated temperature field collected by the 25 HOBO sensors, and the coloured contours are from the simulation with 0.5 m homogeneous spatial resolution (Case D). Overall, the simulation captures the fire-spread behaviour, including the spreading rate and direction of both the fire head and flanks, reasonably well. An under-prediction of the fire spreading rate is observed for the first 100 s after ignition. We attribute these differences to the lack of detailed information about the wind

conditions and limitations of the fire model in representing the turbulence–combustion interaction. This is evident from the comparison of the fire spread behaviour after ignition and fully developed. In the early stage, the fire is driven by the ignition and the ambient wind. As the fire becomes fully established, the fire-induced wind dominates the ambient wind, which diminishes the discrepancy between the simulation and the experiment (Clements et al. 2019).

Fig. 5 compares time histories of velocity and temperature at three different heights on the main tower, corresponding to 20, 10, and 5.8 m AGL. Here, only cases with different horizontal mesh resolutions (A, B, C, and D) are included for comparison. This comparison shows that the simulations capture the highly dynamic flow field and temperature intermittency, which is also observed from the experiment. A rapid increase in temperature is observed



**Fig. 4.** Comparison of isochrones for fire arrival times. Coloured contours are obtained from the simulation with Case D and evaluated for the gas-phase temperature of  $400^{\circ}\text{C}$  at 20 s intervals; black contours are from the experiment (Clements *et al.* 2019).

immediately after the fire front strikes the tower, which induces rapid fluctuations of velocity due to buoyancy. This behaviour is captured by the simulations at all resolutions. In addition, the velocity traces show the correct responses as the fire passes by the tower. An over-prediction of the fire residence time is observed, which we attribute to uncertainties and spatial variability in the fuel load and wind conditions specified in the simulation. To improve the results and assess uncertainties to environmental variables and model sensitivities, further simulations and detailed parametric analyses are required.

From the sample probe data of velocity and temperature, we compute probability density functions (PDFs) to facilitate a statistical comparison, as shown in Fig. 6. These comparisons show that the mean values and general shapes of the distributions predicted by the simulations are in reasonable agreement with experimental measurements, and that the agreement improves with mesh resolutions. To quantify these results, we compared the differences of the first two moments of the streamwise velocity. These results are summarised in Table A1, showing that the largest differences in the mean-flow predictions are observed at the highest measurement location, and with the largest differences observed for Case A (32.7%). The agreement improves with increasing resolution to deviations of 7.1% for Case D. In contrast, the largest differences in the velocity variance are observed for the lowest measurement locations, with deviations of 81.6% for Case A and 65% for Case D. These results suggest that although more accurate characterisation

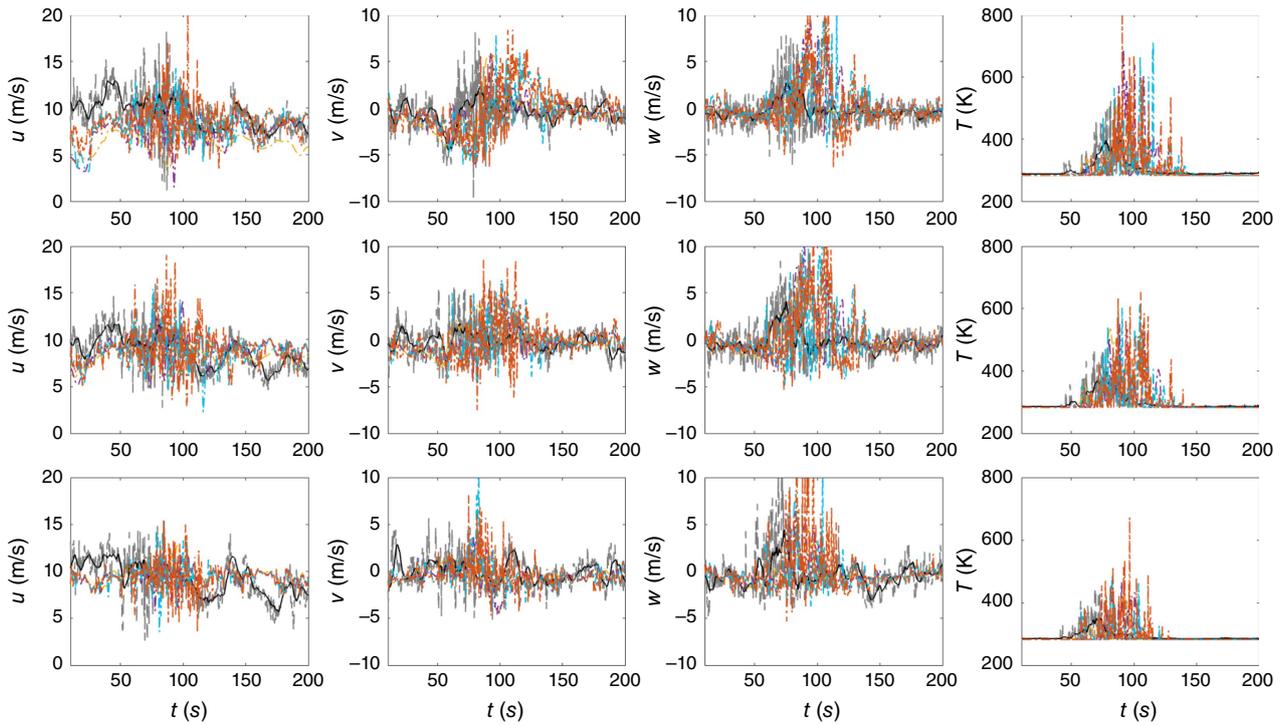
of the experimentally observed wind profile can improve the mean-flow prediction, further improvements in wall models could be beneficial to improve predictions of the turbulence/fire interaction in the viscous boundary layer region.

To examine fire intermittency, we plot the temperature PDFs in log-scale in Fig. 6. Due to the short residence time as the fire passes over the main tower, the distributions are dominated by the ambient temperature. From these comparisons, it can be seen that the simulations predict a broad temperature distribution that is skewed to lower temperatures at ambient conditions. However, it is interesting to note that the PDF for case D at 5.8 m AGL shows a bimodal distribution with a peak in temperature above 700 K, which identifies the increase of gas-phase temperature when the fire passes through the tower.

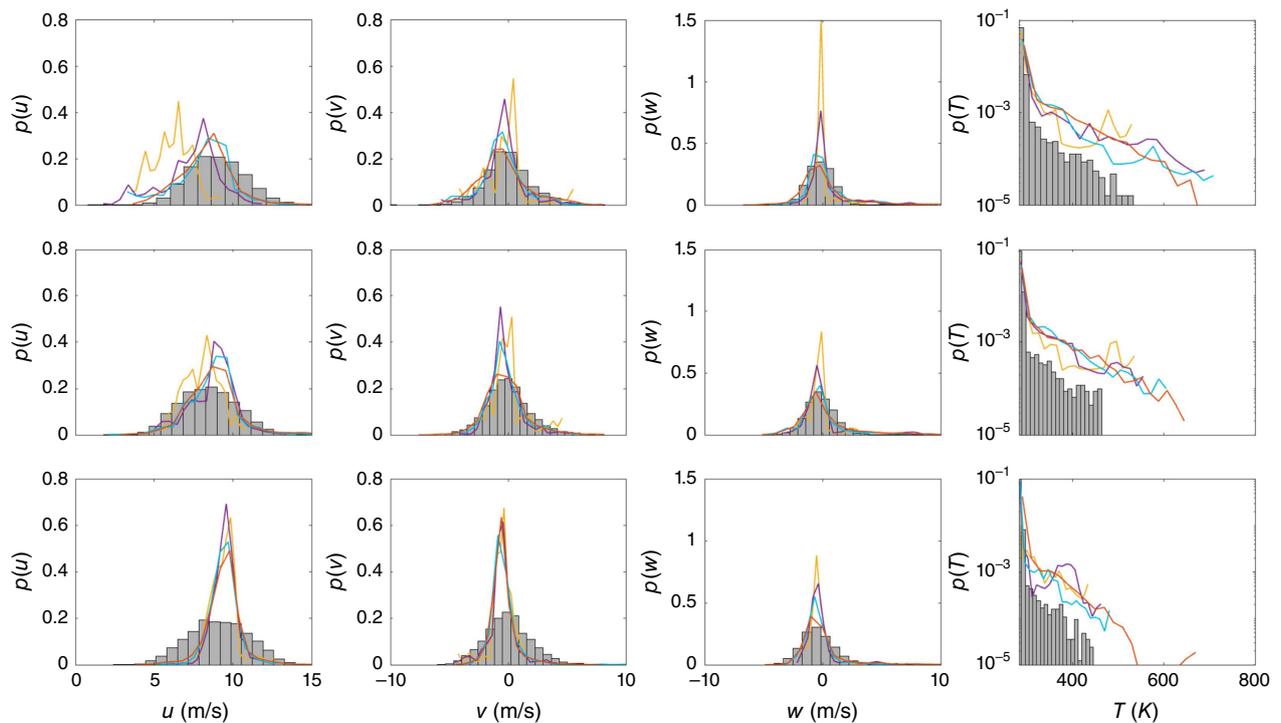
### Statistical analysis of fire behaviour

We proceed by examining global quantities. To this end, we consider the evolution of the heading fire, the fire scar, and the burning rate, as shown in Fig. 7. From results in Fig. 7a, it can be seen that all simulations provide comparable fire-front locations that evolve with a nearly constant spreading rate of 1.6 m/s. These results are in good agreement with the experimental observations (Clements *et al.* 2019), as indicated by the black reference curve in Fig. 7a. The insensitivity of these results with respect to mesh resolution suggest that the spreading rate is mainly dependent on the large-scale turbulence feedbacks between the fire and ambient wind. At the end of the simulations, the prediction in fire front deviates less than 5% from experimental results.

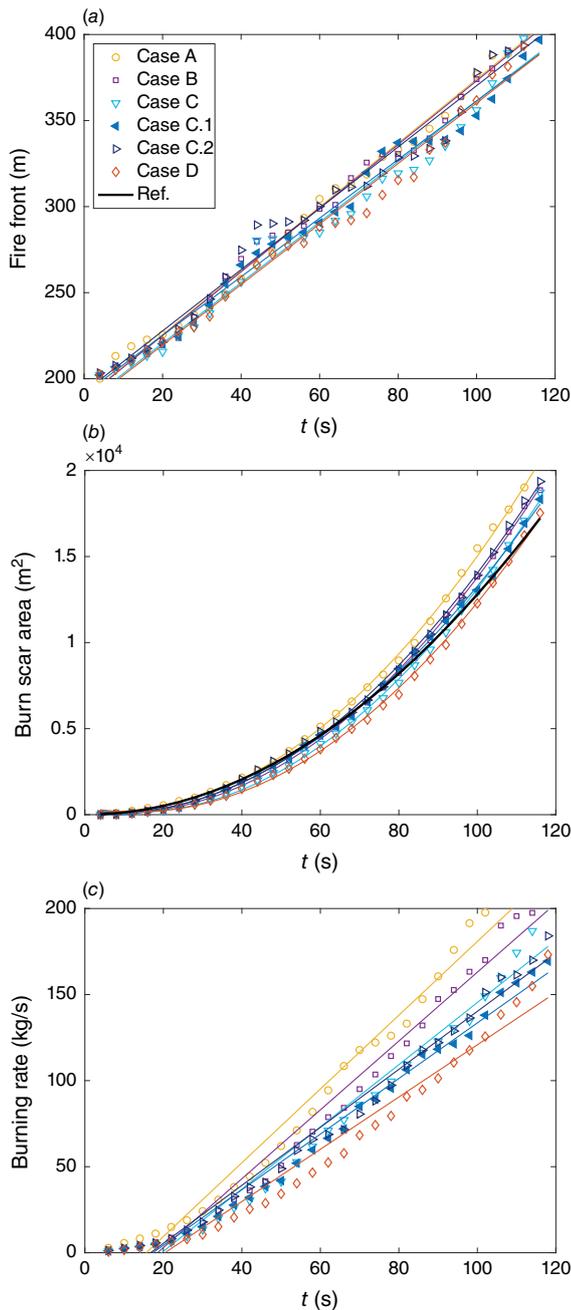
Fig. 7b shows the growth of the fire scar as a function of time. All results converge to a parabolic profile over the first 120 s after ignition. Because the progressive ignition procedure with two fire torches travelling away from each other along a straight line with a speed of 1.6 m/s over the first 110 s of the fire, we can approximate the fire-front location along the baseline of ignition as  $1.6t$  m. Based on the Huygens' principle of elliptic fire behaviour, the location of the fire front along the wind direction can then be approximated by a triangle. The height of the triangle corresponds to the fire spread at the start of the ignition process, which can be approximated as  $\text{ROS} \times t = 1.6t$  m. The area of the fire scar can be therefore approximated as  $0.5 \times 1.6t \times 1.6t = 1.28t^2 \text{ m}^2$ , which is shown as the reference curve in Fig. 7b. This fire behaviour is well captured by all simulations, suggesting that it is largely dominated by the ignition process. In contrast, the burning rate, shown in Fig. 7c, exhibits a more pronounced sensitivity to the horizontal mesh resolution. In particular, a reduction in the burning rate is observed with the increasing horizontal mesh resolution. With an increase of horizontal mesh resolution, small-scale turbulence structures are captured. Fire intermittency as a result of turbulence leads to a reduction in the local residence time (Viegas *et al.* 2022).



**Fig. 5.** Time history of streamwise, lateral, and vertical velocity components and temperature at the main tower at three locations, corresponding to 20 m (top row), 10 m (middle row), and 5.8 m (bottom row) AGL. The black dashed and solid curves represent the original and filtered experimental data, respectively. Colours represent simulations with different resolutions: orange (Case A); violet (Case B); blue (Case C); and red (Case D).



**Fig. 6.** PDFs of streamwise, lateral, and vertical velocity components and temperature at the main tower that are 20 m (top row), 10 m (middle row), and 5.8 m (bottom row) AGL. Results shown by grey histograms are generated from the experimental data. Colours represent simulations with different resolutions: orange (Case A); violet (Case B); blue (Case C); and red (Case D).



**Fig. 7.** Fire front location (a), fire scar area (b), and burning rate (c) for simulations with different mesh resolutions. Colours represent simulations with different resolutions: orange (Case A); violet (Case B); blue (Case C); and red (Case D). Cases C, C.1, and C.2 are labelled with blue at different grey scales. The black curves in Fig. (a) and (b) are references computed with empirical estimation.

Consequently, the solid fuel is consumed slower than it does in a fire that is subject to lower turbulence intensity. As shown in Fig. 3, at the same time after ignition, although the location of the leading edge of the fire is comparable for all simulations, the temperature fluctuations within the fire become more intense with mesh refinement. In addition,

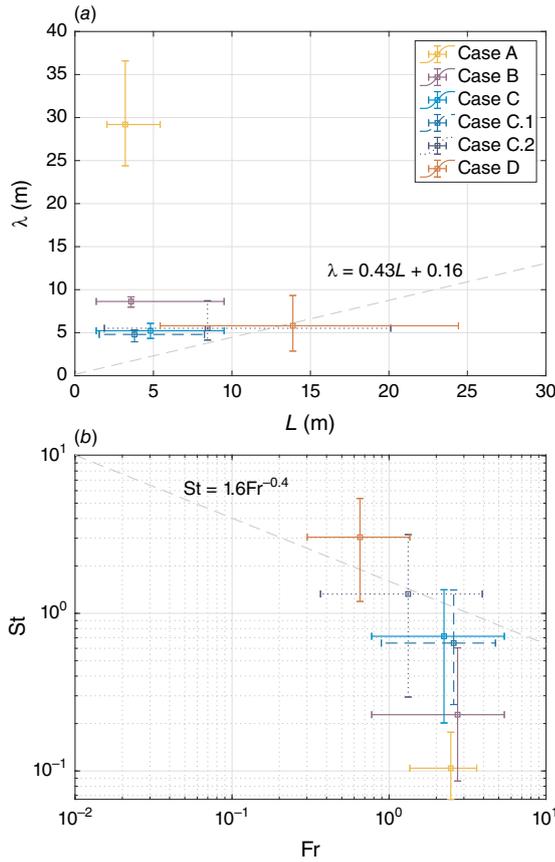
the width of the flame zone increases with increasing mesh refinement, which is consistent with longer average residence times and the presence of residual unburned fuel for longer periods of time as the fire front advances. This observation indicates that the burning rate is not fully converged in the present study and that further refinement is required.

So far, we have largely examined the fire-spread behaviour. To also examine the effects of the mesh resolution on the fire dynamics by buoyancy, we proceed by analysing the ability of the mesh resolution in predicting the buoyant instabilities (Finney *et al.* 2015). In order to relate our analysis to experimental observations, we followed a similar procedure for evaluating the controlling parameters as done by Finney *et al.* (2015), describing the Strouhal number,  $St = fLU^{-1}$ , and Froude number,  $Fr = U^2(gL)^{-1}$ . Here,  $f$  is the frequency,  $\lambda$  is the wavelength,  $L$  is the flame length, and  $U$  is the ambient wind velocity magnitude. Following Finney *et al.* (2021), we estimate the flame length as  $L = h \sec\theta$ , where the flame height  $h$  is determined from the simulation, and  $\theta$  is the tilt angle of the fire with respect to the vertical direction. By analysing our simulation results, the tilt angle was approximated as  $30^\circ$ . The flame height is determined by the vertical coordinates of the fire tip that is identified from the temperature contour at the pyrolysis temperature of 600 K in this study. The wavelength is measured by the average distance between the stripes in the fire front. Results are collected from 80 to 120 s after ignition, with the flame length and wavelength obtained from cross sections aligned and normal to the mean wind direction, respectively, and are shown in Fig. 8a. A wide range of distribution of flame lengths is observed for all simulations, which is due to the unsteadiness and variability of the flame height in response to turbulence. Fig. 8a shows that the buoyancy wavelength remains approximately consistent for horizontal resolutions better than 1 m, showing little sensitivity to vertical resolution (as illustrated by Cases C, C.1, and C.2 having vertical resolution of 0.5, 0.25, and 0.125 m, respectively).

Fig. 8b shows the fire's temporal response at the main tower 20 m AGL. The frequency  $f$  is computed as the inverse of the average period of temperature fluctuation at a specific location. These results show that the frequency and flame height (expressed in terms of flame length in our analysis) exhibit more pronounced sensitivities to the mesh resolution. As a reference, we also include experimentally reported empirical correlations by the black dashed line to guide to reader. We believe that the results presented in this analysis are useful to assess physical models in accurately predicting the buoyant flame dynamics and plume physics, as well as examining sensitivities to capturing these instabilities.

## Computational performance

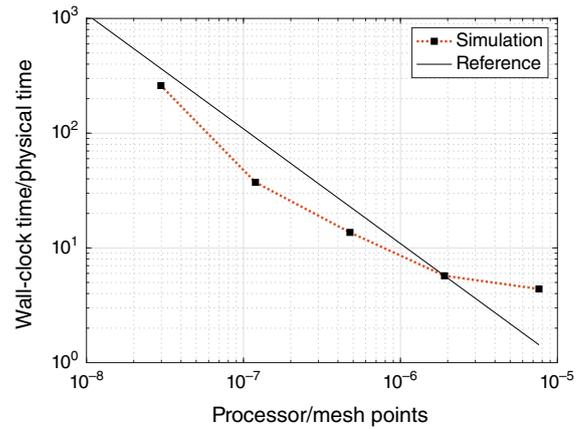
To evaluate the performance of the solver and assess the scalability towards enabling large-scale wildland fire



**Fig. 8.** (a) Distance between fire peaks (represented by the wavelength  $\lambda$ ) versus flame lengths, and (b) Strouhal number in relation to Froude number as measurements of the buoyant fire dynamics in space and time, respectively. Statistics shown in both figures are computed based on results collected between 80 and 120 s after ignition.

simulations, we performed benchmark simulations using 128 TPU cores for the cases A, B, C, and D, and an additional case that had a horizontal mesh resolution of 8 m with a per-core mesh size of  $128 \times 64 \times 16$ . The results are summarised in Fig. 9. For each level of mesh refinement, the number of grid points per core is quadrupled, which provides a maximum number of grid points per core close to 40 million with a memory utilisation of 12 GiB/core. From Fig. 9, for a fixed computational resource, we see a nearly linear speedup with mesh size – except for the case with the smallest number of grid points per processor. We attribute this degradation in performance to the under-utilisation of the MXU compute kernel, which is optimised for performing matrix multiplications of size  $128 \times 128$  per instruction. In addition, in our previous study (Wang et al. 2022a), we have demonstrated that this simulation framework provides linear weak and strong scalability to the full TPU pod.

With relevance to performing large-scale wildland fire simulations, we estimate the largest problem size that we are able to simulate using the currently available TPU



**Fig. 9.** Simulation wall-clock time normalised by physical time as a function of the number of processors allocated per mesh point.

architectures with 8192 cores (TPUv4 pod). Considering a vertical mesh resolution of 1 m in case B and scaling it to a full TPU pod, we estimate being able to simulate domains of  $100 \text{ km}^2$  in size. This is comparable to the burned area of the Northern California Tubbs fire (Martinez et al. 2017), making it feasible to examine the first 3 h during the extreme fire development within 1.3 days of run time (Wang et al. 2022b).

## Conclusions

In this work, we developed a simulation framework utilising TensorFlow programming paradigm and TPU hardware to enable large-scale high-resolution simulations of wildland fires. This simulation framework adopts a quasi-physical model for the representation of the combustion, which is coupled to a large-eddy simulation for the representation of the atmospheric flow field. We performed simulations of the FireFlux II configuration with increasing levels of mesh resolutions, ranging from 4 to 0.5 m horizontally and 0.5 to 0.125 m vertically, and evaluated results against the experiment. The predictions for velocity and temperature at the main tower are compared with available experimental data. Both the temperature projection AGL and the isochrone contours are in reasonable agreement with the experimental observations after the fire is fully established, which demonstrates that the simulation predicts the fire spread in a reasonable manner. Discrepancies at the early stage of the fire after ignition can be attributed to uncertainties in the wind and fuel conditions as well as limitations of the combustion model in representing the combustion processes and turbulence interaction. Results from the mesh-resolution analysis indicate that predictions of intermittent fire behaviour, buoyancy-driven dynamics, and processes that are affected by small-scale turbulent motion benefit from improved mesh refinement.

Results from the scaling analysis show a close to linear scalability of the simulation framework, and conservative estimates indicate that it becomes feasible to perform large-scale simulations of wildland fire scenarios comparable to the Tubbs fire at a spatial resolution of 1 m at acceptable computation time. As such, the capability of generating such high-resolution simulation results for meso-scale wildland fires makes the simulations useful for scientific discovery, forensic analysis, and fire management under realistic conditions and spatio-temporal resolutions.

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**Data availability.** Details on the computational setup (e.g. the inflow boundary conditions) and simulation data are available upon reasonable request to the authors. A preprint of this manuscript is available on Arxiv<sup>1</sup> (Wang et al. 2022c).

**Conflicts of interest.** Craig Clements is an Associate Editor of the International Journal of Wildland Fire. To mitigate this potential conflict of interest he was blinded from the review process and was not involved at any stage in the editing of this manuscript. Other authors declare no conflicts of interest.

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## Appendix I. Governing equations.

The spatial and temporal evolution of the wildland fire through the combustion of solid fuel and the coupling to the atmospheric flow is described by a two-phase model (Linn 1997). In this model, the gas-phase is described by the solution of the Favre-filtered conservation equations for mass, momentum, oxygen-fraction, and potential temperature as:

$$\partial_t \bar{\rho} + \nabla \cdot (\bar{\rho} \bar{\mathbf{u}}) = S_\rho, \quad (1)$$

$$\partial_t (\bar{\rho} \bar{\mathbf{u}}) + \nabla \cdot (\bar{\rho} \bar{\mathbf{u}} \otimes \bar{\mathbf{u}}) = -\nabla \bar{p}_d + \nabla \cdot \bar{\tau} + [\bar{\rho} - \rho(z)] g \hat{\mathbf{k}}_z + \mathbf{f}_D + \mathbf{f}_C, \quad (2)$$

$$\partial_t (\bar{\rho} \bar{Y}_O) + \nabla \cdot (\bar{\rho} \bar{\mathbf{u}} \bar{Y}_O) = \nabla \cdot \bar{\mathbf{j}}_O + \bar{\rho} \bar{\omega}_O, \quad (3)$$

<sup>1</sup>The link to the preprint of this article is: <https://arxiv.org/abs/2212.05141>.

$$\partial_t(\bar{\rho}\tilde{\theta}) + \nabla \cdot (\bar{\rho}\tilde{\mathbf{u}}\tilde{\theta}) = \nabla \cdot \tilde{\mathbf{q}} + \frac{\bar{\rho}\tilde{\theta}}{c_p\tilde{T}} [ha_v(T_s - \tilde{T}) + \dot{q}_r + (1 - \Theta)H_f\tilde{\omega}], \quad (4)$$

where  $\rho$  is the density,  $\mathbf{u}$  is the velocity vector,  $p_d$  is the hydrodynamic pressure,  $\tau$  is the shear stress tensor,  $g$  is the gravitational acceleration constant,  $\hat{\mathbf{k}}_z$  is the unit vector along the gravitational direction,  $f_D = -\bar{\rho}c_d a_v |\tilde{\mathbf{u}}|\tilde{\mathbf{u}}$  is the drag force due to surface vegetation and the drag coefficient is set to  $c_d = 0.01$  (Linn and Cunningham 2005),  $f_C = f\hat{\mathbf{k}}_z \times \bar{\rho}(\tilde{\mathbf{u}} - \mathbf{U}_\infty)$  is the Coriolis force (Siebesma *et al.* 2003) with  $f = -2\Omega \sin \psi$  being the Coriolis coefficient,  $\Omega$  being the rotation rate of the earth and  $\psi$  being the latitude,  $Y_O$ ,  $\mathbf{j}_O$ , and  $\dot{\omega}_O$  are the mass fraction, species diffusion, and source term of the oxidiser  $O$ ,  $\theta$  is the potential temperature,  $\mathbf{q}$  is the heat flux vector,  $T$  is the gas-phase temperature, and  $H_f$  is the heat of combustion. The Favre-filtered value for a generic variable  $\phi$  is defined with the tilde notation as  $\tilde{\phi} = \overline{\rho\phi}/\bar{\rho}$ , where the overbar denotes the Reynolds filtering. The heat exchange with the solid fuel is accounted for by the convective heat transfer, with  $h$  being the convective heat transfer coefficient, and  $a_v$  being the bulk fuel area-to-volume ratio.  $\Theta = 1 - \rho_f/\rho_{f,0}$  is the fraction of the heat release that contributes to the increase of the solid phase temperature (Linn 1997). The shear stress tensor, combining molecular and turbulent transport, is computed as  $\bar{\tau} = 2(\mu + \mu_t)\tilde{S}$ , with  $\tilde{S} = [\nabla\tilde{\mathbf{u}} + (\nabla\tilde{\mathbf{u}})^T]/2 + (\nabla\cdot\tilde{\mathbf{u}})/3$  being the strain rate tensor and  $\mu$  the dynamic viscosity, which is related to the kinematic viscosity with  $\nu = \mu/\rho = 10^{-5} \text{ m}^2/\text{s}$ . In this study, the Smagorinsky model is used to compute the eddy viscosity, which is  $\mu_t = \bar{\rho}\nu_t$  where  $\nu_t = (C_s\Delta)^2|\tilde{S}|$ , with a constant Smagorinsky coefficient  $C_s = 0.18$ . The diffusive flux for oxygen is  $\bar{\mathbf{j}}_O = \bar{\rho}(\alpha + \alpha_t)\nabla\tilde{Y}_O$ , and the heat flux is  $\tilde{\mathbf{q}} = \bar{\rho}(\lambda + \lambda_t)\nabla\tilde{\theta}$ , where turbulent diffusivity and conductivity are computed as  $\alpha_t = \nu_t/Sc_t$  and  $\lambda_t = \nu_t/Pr_t$ , with  $Sc_t$  and  $Pr_t$  being the turbulent Schmidt number for oxygen and the turbulent Prandtl number, respectively.

Using a low-Mach number approximation, we decompose the pressure into hydrostatic and hydrodynamic components,  $p = p(z) + p_d$ , with the hydrostatic pressure computed as  $p(z) = p_0 [1 - gz/(c_p\theta_\infty)]^{1/\kappa}$ , where  $\theta_\infty$  is the potential temperature of the ambient air that is assumed to be a constant,  $p_0$  is the atmospheric pressure on the ground level, and  $\kappa = R/c_p$  is the ratio between the gas constant and specific heat. The temperature is computed as  $\tilde{T} = \tilde{\theta}[p(z)/p_0]^\kappa$ .

The radiation source term is modelled by a grey-gas model as  $\dot{q}_r = -(\sigma k/\zeta)(T_\infty^4 - \tilde{T}^4)$ , with  $\sigma$  being the Boltzmann coefficient,  $k$  being a coefficient that models the turbulence–radiation interaction and is set to 1 for a balanced interaction (Linn 1997),  $T_\infty$  being the ambient temperature, and  $\zeta$  being a characteristic length scale of the fuel elements that is set to 0.5 m for tall grass.

The gas-phase dynamics is coupled to the solid-fuel pyrolysis and the gas-phase reaction. In the present work, we describe the combustion by a one-step global reaction that represents both the pyrolysis of solid fuel and the reaction in the gas phase (Linn 1997):



where  $\nu_F$ ,  $\nu_O$ , and  $\nu_P$  are the stoichiometric coefficients of the fuel  $F$  in the solid phase, the oxygen  $O$  and the combustion products  $P$  in the gas phase, respectively. Denoting  $N$  as the nitrogen that is treated as an inert species in the current formulation, the Favre filtered species mass fractions  $\tilde{Y}_\alpha$  for species  $\alpha \in \{F, O, N, P\}$  satisfy

$$\sum_{\alpha \in \{F, O, N, P\}} \tilde{Y}_\alpha = 1. \quad (6)$$

In the present model, pyrolysis and gas-phase combustion are combined, which is represented through the following reaction rate:

$$\tilde{\omega} = \frac{c_F \rho_F \bar{\rho} \tilde{Y}_O \nu_t \psi_S \lambda_{OF}}{\rho_\infty s_x^2}, \quad (7)$$

where  $c_F = 0.5$  is an empirical scaling coefficient (Linn 1997),  $\rho_F$  is the bulk density of the fuel that is defined as the ratio between the fuel load and the height of the fuel,  $\bar{\rho}$  is the filtered gas phase density,  $\rho_\infty = 1 \text{ kg/m}^3$  is the reference density,  $\nu_t$  is the turbulent diffusivity, and  $s_x = 0.05 \text{ m}$  is an empirical coefficient to parameterise the characteristic turbulence scale. In this model,  $\lambda_{OF}$  is introduced as a coefficient that maximises the reaction rate, which is formulated as:

$$\lambda_{OF} = \frac{\rho_F \bar{\rho} \tilde{Y}_O}{(\rho_F/\nu_F + \bar{\rho} \tilde{Y}_O/\nu_O)^2}. \quad (8)$$

The linear temperature function  $\Psi_S$  in Eqn 7 represents the ignited volume fraction, which is modelled as a function of the gas phase temperature  $\tilde{T}$ :

$$\Psi_S = \max\left(\min\left(\frac{\tilde{T} - T_{\min}}{T_{\max}}, 1\right), 0\right), \quad (9)$$

where  $T_{\min} = 300$  K and  $T_{\max} = 400$  K. The fuel moisture is modelled as the bulk density of liquid water,  $\rho_W$ . The rate of evaporation is modelled as a function of the gas phase temperature, which is similar to the reaction source term and takes the form:

$$\dot{s}_W = -\frac{\rho_{W,0}}{\Delta t} \max(\Psi_W - \max(\Psi_{W,old}), 0), \quad (10)$$

where  $\rho_{W,0}$  is the initial bulk density of moisture,  $\Psi_W = \max\left(\min\left(\frac{\tilde{T} - T_w}{\Delta T}, 1\right), 0\right)$  is the amount of water to be evaporated with  $T_w = 310$  K and  $\Delta T = 126$  K, and  $\max(\Psi_{W,old})$  is the maximum amount of water that has been evaporated.

The solid states, including the fuel load, the moisture content, and the temperature of the fuel, are modelled with the following ordinary differential equations (Linn and Cunningham 2005):

$$d_t \rho_F = -\nu_F \tilde{\omega}, \quad (11)$$

$$d_t \rho_F = \dot{s}_W, \quad (12)$$

$$(c_{p,F} \rho_F + c_{p,W} \rho_W) d_t T_s = \dot{q}_{r,s} + h_{av}(\tilde{T} - T_s) + (H_W + c_{p,W} T_{vap}) \dot{s}_W + (\Theta H_f - c_{p,F} T_{pyr} \nu_F) \tilde{\omega}, \quad (13)$$

where  $c_{p,F}$  and  $c_{p,W}$  are the specific heat of the fuel and liquid water, respectively,  $H_W$  is the heat of vaporisation,  $T_{vap}$  is the temperature of vaporisation, and  $T_{pyr}$  is the temperature at which the solid fuel begins to pyrolyse. Note that the source terms due to combustion and evaporation are incorporated in the gas phase equations through a Lie splitting scheme (Trotter 1959), where the hydrodynamics are integrated following the source terms.

As a result of the combustion and the associated phase exchange, an additional source term is required in Eqn 1 for mass conservation, which is evaluated as  $S_\rho = \nu_F \tilde{\omega} - \dot{s}_W$ . The gas is assumed to be thermodynamically perfect, so the equation of states is modelled by the ideal gas law:

$$p(z) = \bar{\rho} \tilde{R} \tilde{T},$$

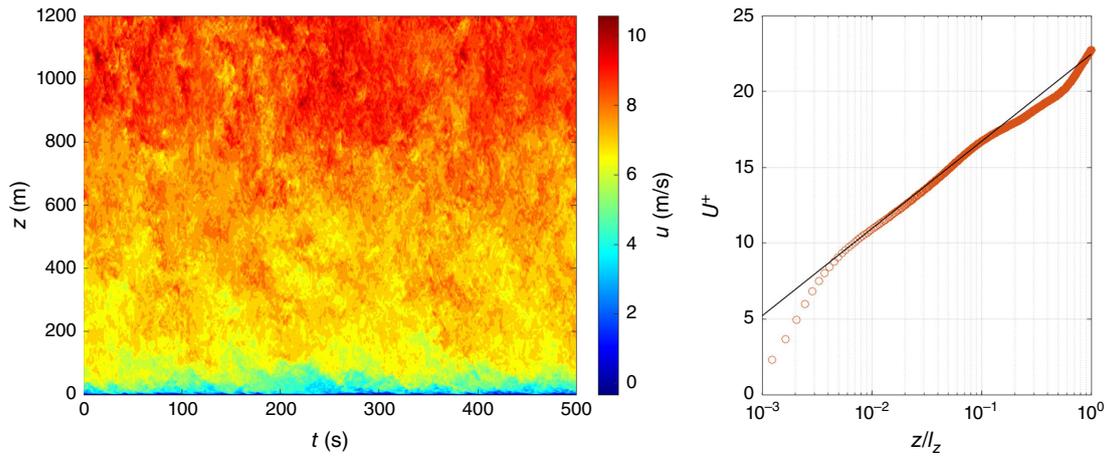
where  $\tilde{R}$  is the gas constant, which is a function of the filtered species mass fractions  $\tilde{Y}_\alpha$ .

**Table A1.** The mean and variance of the streamwise velocity (with deviations to experiments shown in brackets) at the main tower, computed from the PDFs, shown in Fig. 6.

Height (m)	Experiment		Case A		Case B		Case C		Case D	
	Mean	Var.	Mean	Var.	Mean	Var.	Mean	Var.	Mean	Var.
20	9.00	3.154	6.04 (32.7%)	1.42 (55.0%)	7.30 (18.7%)	3.21 (1.9%)	8.00 (10.9%)	3.14 (0.4%)	8.34 (7.1%)	3.12 (1.2%)
10	8.42	3.255	8.00 (5.2%)	1.29 (60.5%)	8.70 (3.2%)	1.98 (39.1%)	8.69 (3.2%)	2.37 (27.2%)	8.80 (4.6%)	3.22 (1.2%)
5.8	9.07	3.642	9.38 (3.4%)	0.67 (81.6%)	9.43 (3.9%)	0.59 (85.2%)	9.42 (3.8%)	0.87 (76.1%)	9.40 (3.7%)	1.28 (65.0%)

## Appendix 2. Turbulent boundary layer structure.

The inflow boundary condition is created from an independent simulation of a neutrally stratified boundary layer. The same computational domain as the fire simulation, which is  $1000 \times 500 \times 1200$  m<sup>3</sup>, is used in this boundary layer simulation, with the inflow–outflow boundary conditions along the streamwise direction being replaced by a periodic boundary condition. To drive this flow, we applied a Coriolis force at a latitude of 31.5°N that corresponds to the location of Texas



**Fig. A1.** The inflow velocity collected from an independent simulation in the same computational domain without fire. The contour shows the time history of the instantaneous streamwise velocity in the middle of the inflow plane, with the horizontal axis being time and the vertical axis being the height of the computational domain. The mean velocity profile shown on the right is compared with the log law of the wall with the horizontal axis being the normalized domain height and the vertical axis being the mean velocity normalized by the friction velocity  $u_\tau$ . The friction velocity is  $u_\tau = 0.36$  m/s, and the corresponding Reynolds number is  $Re_\tau = u_\tau l_z / \nu = 4.32 \times 10^7$ .

where the experiment was conducted, which provides a Coriolis coefficient of  $f = 7.6 \times 10^{-5} \text{ s}^{-1}$  in Eqn 2. A surface roughness of  $z_0 = 0.15$  m is used to model the surface shear stress with the Monin–Obukhov similarity theory. The inflow profiles are collected after 100 flow-through times when the turbulence is fully established and the boundary layer statistics are converged. Based on the result and parameters we specified, we compute the wall shear stress as  $\tau_{i3} = [\kappa(z)|\tilde{\mathbf{u}}(z)| / \ln(z/z_0)]^2 (|\tilde{\mathbf{u}}_i(z)| / |\tilde{\mathbf{u}}(z)|)$ , where  $\kappa = 0.4$  is the von Karman constant, and  $z = 5$  m is the height of the viscous sublayer. The friction velocity in this flow is found to be  $u^* = (\tau_{13}^2 + \tau_{23}^2)^{1/4} = 0.36$  m/s (Moeng 1984). Given that the boundary layer height in this study is  $\delta = l_z = 1200$  m and the kinematic viscosity is  $\nu = 10^{-5} \text{ m}^2/\text{s}$ , the Reynolds number is determined as  $Re_\tau = u_\tau \delta / \nu = 4.32 \times 10^7$  (Yang et al. 2022).

The boundary layer structure is presented in Fig. A1, showing (left) the instantaneous axial velocity field, evaluated at a horizontal location as a function of  $z$  and  $t$ , and (right) the mean velocity profile in inner-scale variables. The viscous sublayer and the logarithmic region are captured below 200 m, providing the representation of the hydrodynamics in regions where the fire–atmosphere interaction is most intense.